

# Effect of water quality on formation of hydrogen peroxide and its behavior on flotation

Alireza Javadi <sup>a,\*</sup>

<sup>a</sup> Department of Engineering, University of Kashan, Kashan, Iran

## Article History:

Received: 16 December 2020.

Revised: 17 August 2021.

Accepted: 24 September 2021.

## ABSTRACT

Water is one of the important parameters in flotation and represents 80–85% of the volume of mineral pulp processed in flotation circuits. In our recent studies revealed was found that sulphide minerals generated  $H_2O_2$  in pulp liquid during wet grinding and also the solids when placed in water immediately after dry grinding but the effect of type of water on the oxidation of pulp components and hence in deteriorating the concentrate grade and recovery in flotation has not been explored yet. In this study, the effect of two types of water on the formation of  $H_2O_2$  as an oxidizing agent stronger than oxygen was investigated. process water is water that is used for a flotation process in Bama Company. It was shown that process water generated  $482 \mu M H_2O_2$  but deionized water generated  $16 \mu M$ . The result shows the recovery of chalcopyrite in pH 6 is 60% and 40% in process water and deionized water respectively. Also, recovery of galena in pH 6 is 30% and 20% in process water and deionized water respectively.

**Keywords:** Hydrogen peroxide, Oxidizing agent, Pyrite, Process water

## 1. Introduction

The billions of gallons of water also a number of chemicals such as collectors, depressants, activators, regulators are used in the flotation process. It is however pertinent to recycle a greater percentage of the used process water within the flotation cycle due to different reasons which include scarcity of freshwater resources as well as to minimize the discharge of the contaminated water to the environment [1-3]. Identifying specific effects of recycled water on the quality of flotation has been a difficult task as there is no common agreement on its impact on flotation, it appears to be detrimental in some studies where the accumulation of species such as calcium, sulphate, carbonate, rest reagents and their oxidation products, thiosalts and other metal ions leads to reduced flotation grade and recoveries [4-6] while in other studies they appear to be beneficial to the flotation process [3-4,7-8]. However, the chemistry of the recycled water is different from that of freshwater because several chemicals and other components such as rest flotation reagents, suspended solid/colloid particles, cations of metals, and anions of organic and inorganic pollutants are now present in the process of water, which inhibit collector adsorption to some extent. It can also be observed that the mineral is generally depressed in process water; this could be due to the presence of a number of dissolved iron [9-11] in the process water which could form hydrophilic layers or iron oxidation species on the surface of chalcopyrite, in addition to the formation of copper hydroxide [12] and iron hydroxide; these hydrophilic species usually play a major role in the depression of chalcopyrite flotation [10]. Our recent studies have illustrated the formation of hydrogen peroxide ( $H_2O_2$ ) by metal-sulfides during grinding in the presence and absence of oxygen [13-16]. In the absence of oxygen, it was found that the pyrite surface is catalytically active and able to break down water molecules to form  $OH^\cdot$  free radical and thereby deriving oxygen in the formation of  $H_2O_2$  from water molecules [11]. The in-situ formation of  $H_2O_2$  and its influence on sulphide

flotation have not been addressed yet.

In this study, the effect of water types on the formation of  $H_2O_2$ , as an oxidizing agent stronger than oxygen was investigated. In mineral processing, this is the first time that the effect of water types during grinding on the formation of  $H_2O_2$  was investigated.

## 2. Materials and methods

Pure chalcopyrite and galena minerals were procured from Gregory, Bottley & Lloyd Ltd., United Kingdom. The minerals were crushed, ground, and classified into different size fractions.  $5 \mu m$  fractions were used in the FTIR study. The chemical composition of the minerals is shown in Table 1. The typical concentration range of various chemical species in Bama Co. process water is shown in Table 2.

**Table 1.** Chemical composition of the minerals used in the studies.

| Minerals     | % Cu | % Fe | % Zn | % Pb  | % S  |
|--------------|------|------|------|-------|------|
| Galena       | 0.2  | 1.38 | 1.26 | 73.69 | 13.5 |
| Chalcopyrite | 25.8 | 29   | 0.54 | 0.22  | 29.5 |

### 2.1. Diffuse reflectance FTIR spectroscopy measurements

The measurement was carried out with the aid of an FTIR spectrometer. The  $5 \mu m$  fraction of the mineral pre-treated at different conditions based on the present study flotation requirements were subjected to FTIR measurements. In each measurement, about 10 mg of  $5 \mu m$  fraction of the mineral is pre-treated at a solids concentration of about 10 mg/100 ml of solution. The pH was adjusted with solutions of  $HNO_3$  and  $KOH$  accordingly. The required concentration of each solution and species was usually prepared followed by the addition of

\* Corresponding author. E-mail address: [alireza.javadi@kashanu.ac.ir](mailto:alireza.javadi@kashanu.ac.ir) (A. Javadi).

the mineral, conditioning for 10 minutes, and addition of other required reagents and species. The pulp was subsequently filtered and the solids left to dry on the filter paper at room temperature. The pH of the suspension after all conditioning prior to filtration is always regarded as the pH of the measurement. Diffuse reflectance infrared Fourier transform (DRIFT) method was used in the measurement with 2.8 wt% concentration in potassium bromide (KBr) matrix. Each spectrum was recorded after 256 scans.

**Table 2.** Chemical species and their concentration range in Bama Co. process water.

| Species              |                 | Concentrations |       |      |
|----------------------|-----------------|----------------|-------|------|
|                      |                 | From           | To    | Unit |
| Sulphate             | SO <sub>4</sub> | 200            | 1700  | mg/l |
| Calcium              | Ca              | 100            | 850   | mg/l |
| Iron                 | Fe              | 0.1            | 1900  | mg/l |
| COD                  | (Cr)            | <30            | 130   | mg/l |
| Nitrogen             | N               | 0.1            | 10    | mg/l |
| Phosphorus           | P               | <0.050         | 0.7   | mg/l |
| Magnesium            | Mg              | 4.3            | 400   | mg/l |
| Manganese            | Mn              | 4.4            | 3100  | µg/l |
| Zinc                 | Zn              | 12             | 4100  | µg/l |
| Aluminium            | Al              | 55             | 51000 | µg/l |
| Cadmium              | Cd              | 0.10           | 5.8   | µg/l |
| lead                 | Pb              | 2.7            | 3500  | µg/l |
| copper               | Cu              | 2.7            | 200   | µg/l |
| Mercury              | Hg              | <0.1           | <0.11 | µg/l |
| Conductivity at 25°C |                 | 91             | 156   | ms/m |

## 2.2. Analysis of hydrogen peroxide

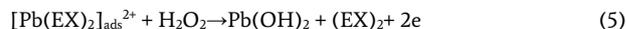
So far, various methods have been used for the measurement of H<sub>2</sub>O<sub>2</sub> in oxidation processes. Such methods use metallic compounds such as titanium oxalate, titanium tetrachloride, and cobalt (II) ion that form colored complexes with H<sub>2</sub>O<sub>2</sub>, which can then be measured spectrophotometrically. The spectrophotometric method using copper (II) ions and DMP has been found to be reasonably sensitive when applied to advanced oxidation processes [17-20]. For the DMP method [21] one milliliter each of DMP, copper (II) sulphate, and phosphate buffer (pH 7.0) solutions were added to a 10 mL volumetric flask and mixed. A measured volume of liquid (filtrate) sample was added to the volumetric flask, and then the flask was filled up with ultrapure water. After mixing, the absorbance of the sample (at 454 nm) was measured with DU® Series 700 UV/Vis Scanning Spectrophotometer. The blank solution was prepared in the same manner but without H<sub>2</sub>O<sub>2</sub>.

## 3. Results and discussion

Table 3 shows H<sub>2</sub>O<sub>2</sub> generation at two water types that processed water produced more H<sub>2</sub>O<sub>2</sub> than deionized water. The effect of different ions on the formation of H<sub>2</sub>O<sub>2</sub> was investigated as shown in Table 3. Table 3 shows that Fe<sup>2+</sup> ions generate substantial H<sub>2</sub>O<sub>2</sub> and Pb<sup>2+</sup> and Zn<sup>2+</sup> give higher concentrations than Fe<sup>3+</sup>, Cu<sup>2+</sup>, Ca<sup>2+</sup> and Mg<sup>2+</sup>. In the presence of dissolved molecular oxygen, ferrous ion forms superoxide (O<sub>2</sub>)<sup>-</sup> (eq. 1) that reacts with ferrous ion to form H<sub>2</sub>O<sub>2</sub> (eqs. 2-4), [22]. This is in agreement with other studies where it was observed that metals-induced formation of free radical generates the superoxide and hydroxyl radical [22-24].



The recovery of chalcopyrite and galena at different pH ranging from 3 to 11.5 in both deionized (DW) and process (PW) water is shown in Fig. 1. It can be seen that the recovery of chalcopyrite decreases generally from low to high pH until pH 10 when it begins to rise again. The recovery of galena decreases generally from pH 3 to pH 6 and rises at pH 7, stabilizes to pH 9 where it begins to rise again. The recovery of both minerals in process water is generally lower than in deionized water. In addition, the recovery of galena in process water is generally lower than in deionized water. In literature reported that reason of depressing of minerals in process water; this could be due to the presence of a number of species including SO<sub>4</sub><sup>2-</sup>, SO<sub>3</sub><sup>2-</sup> [25] dissolved iron [9,11] in the process water which could form hydrophilic layers or iron oxidation species on the surface of chalcopyrite, in addition to the formation of copper hydroxide and iron hydroxide; these hydrophilic species usually play a major role in the depression of chalcopyrite flotation while the strong depressing action of H<sub>2</sub>O<sub>2</sub> on galena may be attributed to its strong oxidizing action on lead xanthate in galena surface giving rise to the oxidation and decomposition of lead xanthate by the reaction of (5) [12, 26]:

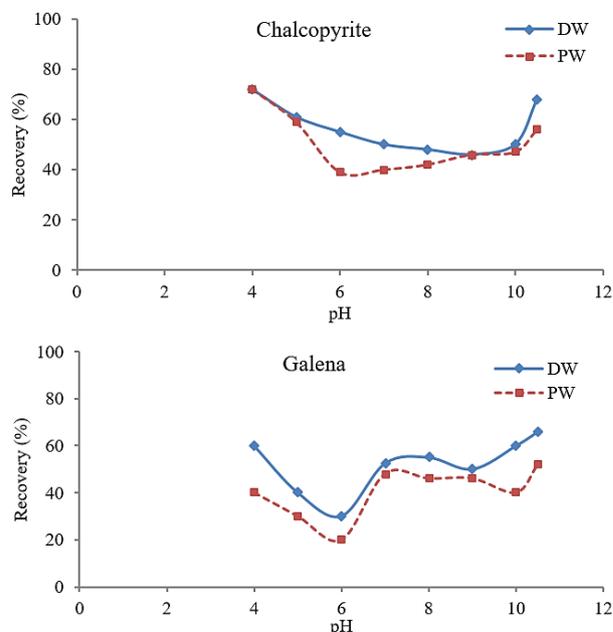


**Table 3.** H<sub>2</sub>O<sub>2</sub> generation at two water types (natural pH, and 22 °C).

|                 | H <sub>2</sub> O <sub>2</sub> (µM) |
|-----------------|------------------------------------|
| Process water   | 482                                |
| Deionized water | 16                                 |

**Table 4.** Effect of metal ions on H<sub>2</sub>O<sub>2</sub> generation at two initial concentrations (conditioning time 1 h, natural pH, and 22 °C).

| Concentration of ions | H <sub>2</sub> O <sub>2</sub> (µM) |       |
|-----------------------|------------------------------------|-------|
|                       | 1 mM                               | 10 mM |
| water                 | 0                                  | 0     |
| Fe <sup>2+</sup>      | 551                                | 465   |
| Fe <sup>3+</sup>      | 4.1                                | 60    |
| Cu <sup>2+</sup>      | 0.6                                | 15    |
| Pb <sup>2+</sup>      | 13                                 | 96    |
| Ca <sup>2+</sup>      | 0                                  | 6     |
| Mg <sup>2+</sup>      | 0                                  | 0     |
| Zn <sup>2+</sup>      | 0.6                                | 88    |



**Fig. 1.** Recovery of chalcopyrite and galena at different pHs in deionized and processed water.

Therefore, at certain pH and  $H_2O_2$  concentrations, the complete decomposition of lead xanthate preadsorbed on galena renders galena surface hydrophilic and depression of galena, whereas the dioxanthogen prefixed on chalcopyrite remains stable, which confers chalcopyrite surface hydrophobic and floatable, which was proved by voltammogram method [27].

### 3.1. Diffuse reflectance FTIR studies

Since  $H_2O_2$  can oxidize surfaces, the solid fraction was subjected to FTIR analysis to examine the surface species. The FTIR spectra of  $-5 \mu m$  pure chalcopyrite and chalcopyrite treated with  $H_2O_2$  at different times are shown in Fig. 2. Untreated chalcopyrite spectrum exhibits two broad bands centered around  $1009 \text{ cm}^{-1}$  and  $467 \text{ cm}^{-1}$ , and weak bands at  $1189$ ,  $796$ ,  $684$ ,  $631$ , and  $517 \text{ cm}^{-1}$  frequency. In addition to these bands, the oxidized chalcopyrite sample display bands at  $3622$ ,  $3554$ ,  $3390$ , and  $1090 \text{ cm}^{-1}$ . The intensity of all bands in the  $H_2O_2$  treated sample spectra increases with increasing time of treatment, implying that these bands relate to surface oxidized sulfoxyanion and hydroxide species. The bands at  $1189$  and  $1009 \text{ cm}^{-1}$  can be assigned to S–O stretch vibrations in sulphate and sulphite structures respectively, while the band at  $631 \text{ cm}^{-1}$  represents S–O bend vibrations. The superficial iron oxy-hydroxide species display bands in the  $796$ – $630 \text{ cm}^{-1}$  region and iron sulphate at  $467 \text{ cm}^{-1}$ ; however, the several bands around  $470$  and  $780 \text{ cm}^{-1}$  could also arise due to Si–O vibrations caused by silicate impurity in the sample. The bands in the region  $3000$ – $3700 \text{ cm}^{-1}$  of the  $H_2O_2$  treated sample characterize O–H stretching vibrations of surface hydroxyl groups. The spectra with increasing time of  $H_2O_2$  treatment and in process water, the intensity of O–H bands increased. While comparing the pure chalcopyrite spectrum to the spectra oxidized by  $H_2O_2$ , it is clear that the pure chalcopyrite sample used in experiments is partially oxidized.

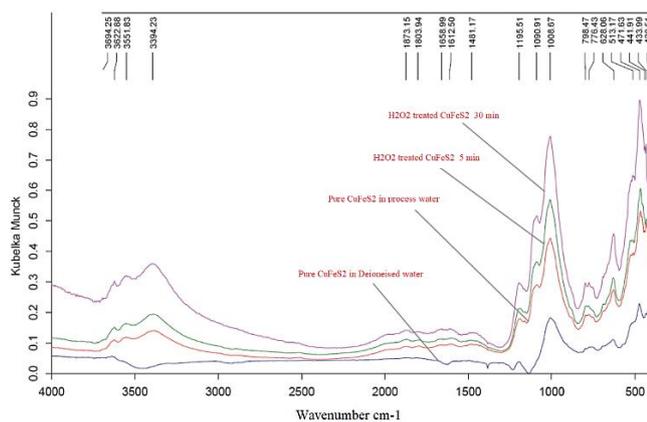


Fig. 2. Pure and  $H_2O_2$  treated chalcopyrite DRIFT spectra.

The diffuse reflectance spectrum of the  $-5 \mu m$  galena powder sample is shown in Fig. 3. The spectra of the same sample conditioned with  $H_2O_2$  at different times are also presented in this figure. Since galena exhibits a fundamental vibration below  $200 \text{ cm}^{-1}$ , the several bands seen in the spectrum of the pure sample are due to oxidized species on the surface. An increase in the intensity of these bands when the sample is treated with an  $H_2O_2$  oxidant substantiates that these bands are characteristic of oxidized species present on the sample. The oxidized surface state of galena mainly consists of lead sulphate and thiosulphate, and lead carbonate. The bands at  $598$ ,  $629$ ,  $1051$ ,  $1093$ , and  $1160 \text{ cm}^{-1}$  can be assigned to S–O vibrations in lead sulphate. Lead thiosulphate bands that could appear at about  $985$  and  $1120 \text{ cm}^{-1}$  were not noticed in the spectra. Absorption bands characteristic of C–O vibrations in lead carbonate are seen at about  $679$ ,  $838$ ,  $1051$ ,  $1409$ , and  $1425 \text{ cm}^{-1}$ . With increasing time of  $H_2O_2$  treatment and in process water, the intensity of sulphate bands increased. While comparing the pure galena spectrum to the spectra oxidized by  $H_2O_2$ , it is clear that the pure galena sample used in experiments is partially oxidized.

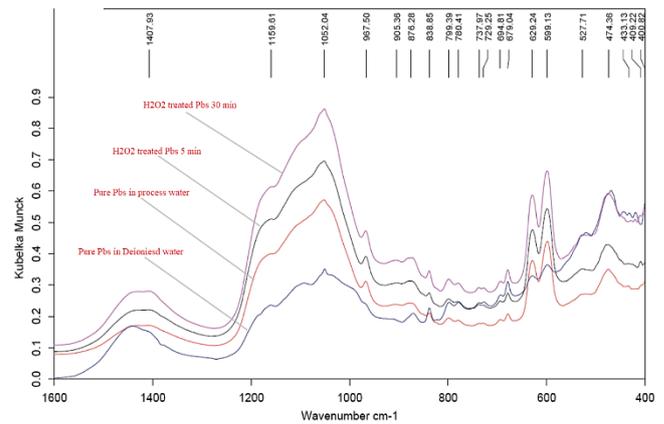


Fig. 3. DRIFT spectra of pure and  $H_2O_2$  treated galena.

The spectra of chalcopyrite treated with xanthate in deionized and process waters after subtracting the pure mineral spectrum conditioned at the same experimental pH 10.5 without xanthate are shown in Fig. 4. Within a maximum xanthate concentration of  $5 \times 10^{-5} \text{ M}$  used, the difference spectra with increasing xanthate concentration in deionized water show three prominent bands at  $1201$ ,  $1157$ , and  $1098 \text{ cm}^{-1}$ , and a band at  $1011 \text{ cm}^{-1}$  appears at a higher concentration. These bands are associated with adsorbed xanthate species where the higher intensity band  $1098 \text{ cm}^{-1}$  can be assigned to C–O–C vibrations and the bands at  $1201$  and  $1011 \text{ cm}^{-1}$  are due to S–C–S and C–O–C stretching vibrations [28–31]. The bands characteristic of copper xanthate ( $1157 \text{ cm}^{-1}$ ) and dioxanthogen ( $1201 \text{ cm}^{-1}$ ) are observed. In process water, the S–O stretching band ( $1008 \text{ cm}^{-1}$ ) dominates over xanthate species bands, weak and low-intensity bands ( $1181$ ,  $1144$ ,  $1084 \text{ cm}^{-1}$ ) inferring lower adsorption of xanthate.

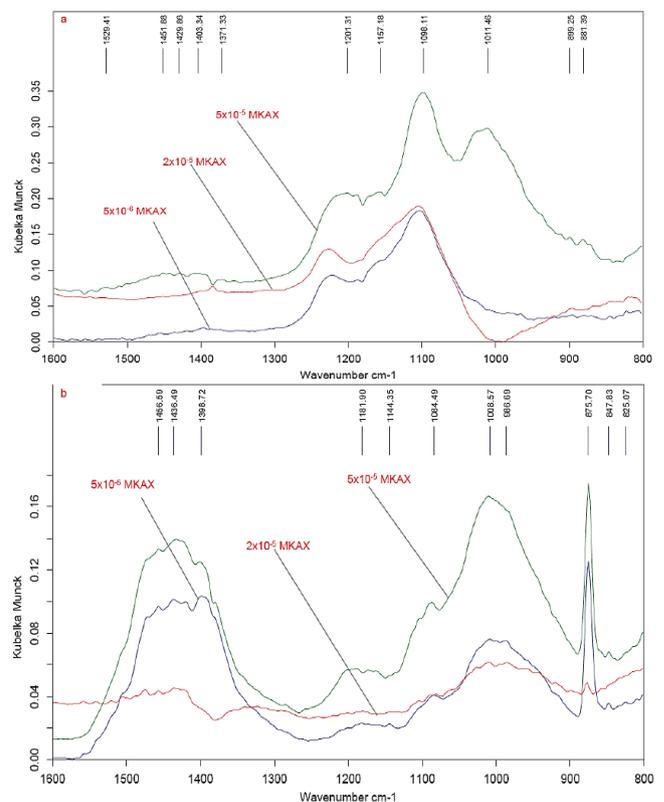
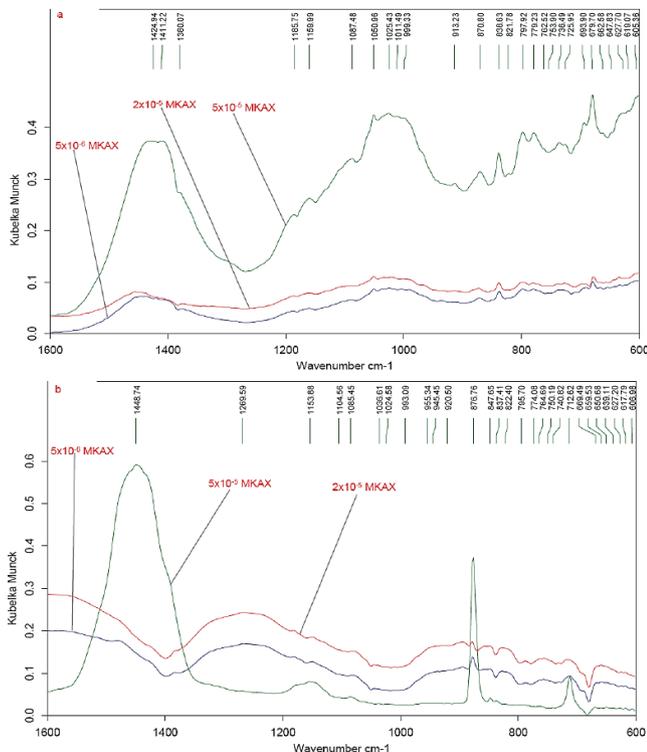


Fig. 4. Difference DRIFT spectra of chalcopyrite treated at different xanthate concentrations at pH 10.5 in deionized (a) and process (b) waters after subtracting the respective pure mineral reference spectrum.



**Fig. 5.** Pure mineral subtracted from galena treated at different xanthate concentrations at pH 10.5 in deionized (a) and process (b) waters.

Spectra of galena after interaction with amyl xanthate at  $5 \times 10^{-6}$ ,  $2 \times 10^{-5}$ , and  $5 \times 10^{-5}$  M concentrations in deionized (a) and process (b) waters are shown in Fig. 5. These were the difference spectra after subtracting the mineral spectrum from the xanthate treated spectra. In deionized water, the spectra exhibit the C-O-C and S-C-S symmetric stretching vibration band at  $1187 \text{ cm}^{-1}$  and the stretching vibration band of the S-C-S group at  $1024 \text{ cm}^{-1}$  [28-31]. Comparing the corresponding bands in the lead amyl xanthate (1:2) compound, these bands are shifted from  $1220 \text{ cm}^{-1}$  to a lower value of  $1187 \text{ cm}^{-1}$  and from  $1022$  to  $1024 \text{ cm}^{-1}$ . These bands can be assigned to a monocoordinated form of lead xanthate. Furthermore, increasing xanthate concentration to  $5 \times 10^{-5}$  M, the intensity of these bands is seen to increase illustrating increased amyl xanthate adsorption on galena surface. However, the lead sulphate ( $1160$ ,  $1132$ ,  $1025 \text{ cm}^{-1}$ ) and lead carbonate ( $1051$ ,  $838 \text{ cm}^{-1}$ ) bands although diminished can be seen in these spectra. The surface oxidized products of galena are expected to be removed during the abstraction of xanthate. The presence of oxidation products indicates that the maximum initial xanthate concentration of  $5 \times 10^{-5}$  M used is not adequate to form monolayer coverage. In process water and at low xanthate concentrations of  $5 \times 10^{-6}$  and  $2 \times 10^{-5}$  M, the spectra show only the oxidized substrate bands and are devoid of xanthate bands. The absence of xanthate bands could be that xanthate is in complex formation with the metal ions in process water. However, at the  $5 \times 10^{-5}$  M xanthate concentration spectrum, xanthate bands can be seen. The presence of positive and negative lead sulphate and lead carbonate bands illustrates the different levels of surface oxidation compounds in the xanthate treated galena spectra compared to the mineral spectrum that was subtracted.

#### 4. Conclusion

The recovery of both minerals in process water is generally lower than in deionized water. In addition, the recovery of galena in process water is generally lower than in deionized water. In literature reported that reason of depressing of minerals in process water; this could be due to the presence of a number of species including  $\text{SO}_4^{2-}$ ,  $\text{SO}_3^{2-}$  dissolved iron

in the process water which could form hydrophilic layers or iron oxidation species on the surface of chalcopyrite, in addition to the formation of copper hydroxide and iron hydroxide; these hydrophilic species usually play a major role in the depression of chalcopyrite flotation while the strong depressing action of  $\text{H}_2\text{O}_2$  on galena may be attributed to its strong oxidizing action on lead xanthate in galena surface giving rise to the oxidation and decomposition of lead xanthate. This study showed that  $\text{Fe}^{2+}$  ions in process water generate substantial. In the presence of dissolved molecular oxygen, ferrous ion forms superoxide ( $\text{O}_2^-$ ) that reacts with ferrous ion to form  $\text{H}_2\text{O}_2$ . The DRIFT spectra of chalcopyrite and galena pure samples showed that the surfaces are partially oxidized depicting surface sulfooxy, oxyhydroxide, and carbonate species absorbance bands. These oxidized species bands are evidenced by the bands that developed when the samples are oxidized with  $\text{H}_2\text{O}_2$  oxidant.

#### REFERENCES

- [1] Broman, P.G. (Editor), 1980. Water reuse at sulphide ore concentrators in Sweden: practice, experience and current developments. In: M.J Jones, Editor, Complex Sulphide Ores. Institution of Mining and Metallurgy, London, 28-39 pp.
- [2] Rao, S.R. and Finch, J.A., 1989. A review of water re-use in flotation. Minerals Engineering, 2(1): 65-85.
- [3] Liu, L., Rao, S.R. and Finch, J.A., 1993. Technical note laboratory study of effect of recycle water on flotation of a Cu/Zn sulphide ore. Minerals Engineering, 6(11): 1183-1190.
- [4] Basilio, C.I., Kartio, I.J. and Yoon, R.H., 1996. Lead activation of sphalerite during galena flotation. Minerals Engineering, 9(8): 869-879.
- [5] Haran, N.P., Boyapati, E.R., Boontanjai, C. and Swaminathan, C., 1996. Kinetics Studies on Effect of Recycled Water on Flotation of Copper Tailings from Benambra Mines, Victoria. Wiley Subscription Services, Inc., A Wiley Company, pp. 197-211.
- [6] Levay, G., Smart, R.S.C. and Sinner, W.M., 2001. The impact of water quality on flotation performance. The Journal of The South African Institute of Mining and Metallurgy 101(2): 69-75.
- [7] Chen, J.-m., Liu, R.-q., Sun, W. and Qiu, G.-z., 2009. Effect of mineral processing wastewater on flotation of sulfide minerals. Transactions of Nonferrous Metals Society of China, 19(2): 454-457.
- [8] Bakalarz, A., Duchnowska, M., Luszczkiewicz A., The effect of process water salinity on flotation of copper ore from Lubin mining region, E3S Web of Conferences 18 , 01007 ( 2017 )
- [9] Kant, C., Rao, S.R. and Finch, J.A., 1994. Distribution of surface metal ions among the products of chalcopyrite flotation. Minerals Engineering, 7(7): 905-916.
- [10] Peng, Y., Grano, S., Fornasiero, D. and Ralston, J., 2003a. Control of grinding conditions in the flotation of chalcopyrite and its separation from pyrite. International Journal of Mineral Processing, 69(1-4): 87-100.
- [11] Peng, Y., Grano, S., Fornasiero, D. and Ralston, J., 2003b. Control of grinding conditions in the flotation of galena and its separation from pyrite. International Journal of Mineral Processing, 70(1-4): 67-82.
- [12] Fullston, D., Fornasiero, D. and Ralston, J., 1999. Zeta potential study of the oxidation of copper sulfide minerals. Colloids and Surfaces A: Physicochemical and Engineering Aspects, 146(1-3): 113-121.
- [13] Javadi Nooshabadi, A. & Hanumantha Rao, K., (2013). Formation

- of hydrogen peroxide by pyrite and its influence on flotation. *Minerals Engineering*, Volume 49, p. 128–134.
- [14] Javadi Nooshabadi, A. & Hanumantha Rao, K., (2013). Formation of hydrogen peroxide by chalcopyrite and its influence on flotation. *Minerals and Metallurgical Processing*, Volume 30(4), p. 212-219.
- [15] Javadi Nooshabadi, A. & Hanumantha Rao, K., (2013). Formation of hydrogen peroxide by sphalerite. *International Journal of Mineral Processing*, Volume 125, p. 78–85.
- [16] Javadi Nooshabadi, A. & Hanumantha Rao, K., (2014). Formation of hydrogen peroxide by galena and its influence on flotation. *Advanced Powder Technology*, Volume 25(3), p. 832-839
- [17] Sunder, M.; Hempel, D. C., 1997. Oxidation of tri- and perchloroethene in aqueous solution with ozone and hydrogen peroxide in a tube reactor, *Water Research*. 31, 33-40.
- [18] Leitner K. , N.; Dore', M., 1997. Mechanism of the reaction between hydroxyl radicals and glycolic, glyoxylic, acetic and oxalic acids in aqueous solution: Consequence on hydrogen peroxide consumption in the *Water Research*. 31, 1383- 1397.
- [19] Roche, P.; Prados, M., Removal of pesticides by use of ozone or hydrogen peroxide, *Ozone: Science & Engineering*. Eng. 1995, 17, 657-672.
- [20] Kosaka K., Yamada H., Matsui S., Echigo S., Shishida K., 1998. A Comparison among the Methods for Hydrogen Peroxide Measurements To Evaluate Advanced Oxidation Processes: Application of a Spectrophotometric Method Using Copper(II) Ion and 2,9-Dimethyl-1,10-phenanthroline, *Environ. Sci. Technol.*, 32, 3821-3824.
- [21] Baga, A. N.; Johnson G. R. A.; Nazhat, N. B.; Saadalla-Nazhat, R. A., 1988. *Anal. Chim. Acta*, 204, 349-353.
- [22] Jones, G., van Hille, R.P., Corin, K.C., Harrison, S.T.L., 2011. The generation of toxic reactive oxygen species (ROS) from mechanically activated sulphide concentrates and its effect on thermophilic bioleaching, *Minerals Engineering* 24(11):1198-1208.
- [23] Jones, G., van Hille, R.P., Harrison, S.T.L., 2012. Reactive oxygen species generated in the presence of fine pyrite particles and its implication in thermophilic mineral bioleaching *Appl. Microbiol. Biotechnol.* doi: 10.1007/s00253-012-4116-y.
- [24] Volk, C.; Roche, P.; Renner, C.; Paillard, H.; Joret, J. C., Effects of ozone-hydrogen peroxide combination on the formation of biodegradable dissolved organic carbon, *Ozone: Science & Engineering*. 1993, 15, 405-418.
- [25] Houot, R. and Duhamet, D., 1992. The use of sodium sulphite to improve the flotation selectivity between chalcopyrite and galena in a complex sulphide ore. *Minerals Engineering*, 5(3-5): 343-355.
- [26] Mobarhan, M., Ahmadi, R., Karimi, R.Gh, 2021, Comparison of the Effect of Tap Water and Process Water on the Galena and Sphalerite Minerals Flotation, *Journa of Mineral Resources Engineering*, Vol 6., 71-81.
- [27] Hu, Y., Sun, W., Wang, D., 2009, *Electrochemistry of Flotation of Sulphide Minerals*, book, Springer-Verlag Berlin Heidelberg, Jointly published with Tsinghua University Press.
- [28] de Donato, P. et al., 1999. Chemical surface modifications of sulphide minerals after comminution. *Powder Technology*, 105(1-3): 141-148.
- [29] Persson, P. and Persson, I., 1991. Interactions between sulfide minerals and alkylxanthate ions 2. A vibration spectroscopic and atomic absorption spectrophotometric study of the interactions between sphalerite and copper-activated sphalerite and ethyl- and n-decylxanthate ions in aqueous and acetone solutions. *Colloids and Surfaces*, 58(1-2): 149-160.
- [30] Leppinen, J.O., 1990. FTIR and flotation investigation of the adsorption of ethyl xanthate on activated and non-activated sulfide minerals. *International Journal of Mineral Processing*, 30(3-4): 245-263.
- [31] Leppinen, J.O., Basilio, C.I. and Yoon, R.H., 1989. In-situ FTIR study of ethyl xanthate adsorption on sulfide minerals under conditions of controlled potential. *International Journal of Mineral Processing*, 26(3-4): 259-274.